

Solution to Homework 7, Problem 1

Parts a.-k. - Original design

Design parameters

Design flow rate	Q	0.0088	m ³ /s
Reactor volume	V	25	m ³
Influent COD concentration	S _{in}	300	mg COD/L
Solids concentration of recycled sludge	X _R	12000	mg VSS/L
Clarified effluent from secondary clarifier	X _e	15	mg VSS/L
Safety factor	SF	20	

Part I. - Redesign

0.0088	m ³ /s
50	m ³
300	mg COD/L
12000	mg VSS/L
15	mg VSS/L
80	

Kinetic constants:

Maximum specific growth rate	μ _{max}	9.6	day ⁻¹
Half-saturation constant	K _S	75	mg/L as COD
Cell yield	Y	0.4	g VSS/g COD
Endogenous respiration rate	k _e	0.096	day ⁻¹

Computed characteristics

a.	Hydraulic residence time	t _R	0.8	hours
b.	Minimum solids retention time	θ _{c,min}	2.5	hours
	Washout solids retention time	θ _{c,w}	3.16	hours
c.	Design solids retention time (sludge age)	θ _c	51	hours
	Design solids retention time (sludge age)	θ _c	2.1	days
d.	Reactor biomass concentration	X	6288	mg VSS/L
e.	Effluent substrate concentration	S	4.7	mg COD/L
	Efficiency	E	98.4	percent
f.	Substrate utilization rate	U	1.43	g COD/g VSS/day
g.	Food:microorganism ratio	F/M	1.45	g COD/g VSS/day
h.	Recycle ratio	r	1.08	
	Recycle flow rate	Q _R	0.010	m ³ /s
i.	Sludge wasting rate	Q _W	0.00025	m ³ /s
		Q _W /Q	2.8%	
j.	Sludge production rate	P	3.1	kg VSS/hr

1.6	hours
2.5	hours
3.16	hours
202	hours
8.4	days
8447	mg VSS/L
1.7	mg COD/L
99.4	percent
0.54	g COD/g VSS/day
0.54	g COD/g VSS/day
2.36	
0.021	m ³ /s
0.00016	m ³ /s
1.9%	
2.1	kg VSS/hr

- k. This plant has a high F/M ratio and short SRT. As such, it would be classified as a high-rate aeration plant. Such a plant can work, but is not compatible with the intended low level of maintenance planned for this facility. More bluntly, this plant is a disaster waiting to happen!
- l. The plant needs to be redesigned as a low-rate AST plant. A design safety factor of SF = 100 is more appropriate and would raise the SRT to 8.4 days, which is more consistent with a low-maintenance, low-rate treatment plant. However, raising the SRT has the perverse effect of raising the biomass concentration (X) which in turn raises the F/M ratio (see Lecture 19, Equation 41). To lower the F/M ratio, we can increase the tank volume, which increases t_R, which in turn lowers F/M according to Equation 30.